Natural Convection in an Enclosure: Effect of Magnetic Field Dependent Thermal Conductivity

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Abstract - In this paper, the natural convection heat transfer process is investigated inside an annular enclosure filled with a magnetic nanofluid (Fe₃O₄ magnetic nanoparticles dispersed in Kerosene). A uniform magnetic field (*H*) is applied along the axial direction of the enclosure. Thermal conductivity (*k*) is considered as a function of magnetic field. A nonlinear relationship between magnetic field and thermal conductivity in the magnetic nanofluid (MNF) is assumed and interpolated. Finite element method is utilized to solve the governing equations and calculate the Nusselt number and it is presented as a function of volume fraction and magnetic field strength. The results show the significant effect of applied magnetic field on heat transfer rate, more specifically on Nu, in the enclosure when higher volume fractions of nanoparticles are used. Thermal conductivity enhancement as a result of using magnetic field can be used for various applications such as thermal energy storage in which the heat transfer needs to be accurately controlled.

Keywords: Magnetic nanofluid (MNF), Thermal conductivity, Lorentz force, Natural convection

Nomenclature

В	Magnetic flux density [T]
\overline{B}_{N}	Component of magnetic flux density
\overline{C}_n	Heat capacitance at constant temperature [J/kg.K]
d^{p}	Diameter of nanoparticle [nm]
d _n	Diameter of nanoparticles [nm]
Ē	Electrical field [V/m]
Ĩ	Current density [A/m2]
K	Pyromagnetic coefficient
k	Thermal conductivity [W/m K]
L.	Characteristic Length [m]
M	Magnetization respect to temperature
T	Temperature [K]
<i>x.v</i>	Space coordinates [m]
<i>u.v</i>	Velocity components in the x and y directions $[m/s]$
Greek symbols	
α	Thermal diffusivity [m2/s]
β	Coefficient of thermal expansion [1/K]
Ŷ	Magnetic Susceptibility
v	Kinematic viscosity [m2/s]
ú	Dynamic viscosity [kg/ms]
σ	Electrical conductivity $[(\Omega, m)^{-1}]$
0	Density [kg/m3]
ø	Volume fraction [%]
Subscripts	
c	Cold
ĥ	Hot
си	Curie
f	Fluid
S	Solid
nf	Nanofluid

1. Introduction

Heat transfer enhancement has been a challenging topic for researchers for many years to enhance the efficiency of many applications such as cooling and electronic equipments and solar systems. Numerous studies have been carried out on passive and active heat transfer systems to increase their efficiencies [1, 2]. One of the effective ways to improve the heat transfer rate in fluids is adding conductive nanoparticle to the fluid [3]. In addition, the use of magnetic field in thermal process provides more opportunities for a wide range of applications such as thermal energy storage systems, magnetic refrigeration systems, and thermal batteries [4]. Beside the heat transfer enhancement, the main advantage of MNF is capability of being controlled via external magnetic field. Such a unique behaviour of this type of fluid (MNF) in the presence of a magnetic field creates opportunities in different applications like biomedical, electrical, and thermal engineering systems.

Magnetic nanoparticles are suspended in the carrier/base fluid and subjected to the gravitational and magnetic field; thus, the particle sedimentation is a factor that has to be taken into account. Also, the interaction and forces between nanoparticles, which causes Brownian motion, directly depend on size of the nanoparticle. In some researches the effect of Brownian motion are considered, whereas, in the others it was neglected. A summary of literature reviewed on thermal enhancement using magnetic nanofluids for different enclosures is tabulated in Table 1.

Author(s)	Year	Geometry	Material	Outcome Contribution summary	
Mukhopadhyay et. al. [6]	2005	Square enclosure	Water/oil-based	Boussinesq assumption heat transfer rate improved	
Blums et. al. [7]	2008	Cylinder (50 mm length and 5mm diameter)	Porcelain cylinder oleic acid	Thermomagnetic investigation body forces- possible to increase R_{a_m} exceed 20 times more than R_{a_T}	
Ming et. al. [8]	2009	Annulus	Water-based Fe ₃ O ₄	Optimal working fluid ratio (53.5%) for the specific geometry	
Zablotsky et. al. [9]	2009	Rectangular	Ferrofluid, Mn-Zn particle	Cooling via thermomagnetic convection if heat source is in maximal magnetic field intensity	
Fang et. al. [10]	2009	Cubic micro enclosure	Not specified	Direct relation between chainlike cluster and particle volume fraction	
Ashouri et. al. [11]	2010	Square cavity	Various ferrofluids	General correlation for Nu and its error	
Aminfar et. al. [12]	2012	Triangular enclosure	CuO-Water	Studies on different <i>Ra Ha</i> numbers to obtain highest heat transfer rate	
Sheikholeslami et. al. [13]	2014	L-shaped enclosure	Al ₂ O ₃	Heat transfer using control volume using KKL by inclination angle	
Mustafa et. al. [14]	2014	Vertical channel	Not specified	Mathematical model for peristaltic motion in vertical channel	
Rashidi et. al. [15]	2015	Square enclosure (obstacle embedded)	Not specified	Flow separation via magnetic field	

Table 1: Summary of previous studies on MNF with magnetic field for different geometry.

It can be seen from the Table 1 that many numerical investigations are carried out for various enclosure geometries. Based on the achievements of previous studies in Table 1, thermal conductivity (k) is an important parameter to improve the heat transfer rate. To the best of the authors' knowledge, no numerical study is conducted in which thermal conductivity was a function of both magnetic field (H) and volume fraction (ϕ). Thus, in this study we proposed an annular enclosure with specific geometry subjected to uniform magnetic field and analysed the heat transfer. Fig. 1 shows the enclosure filled with pure kerosene as a base fluid and Fe₃O₄ as magnetic nanoparticle. The material of the enclosure is acrylic glass and inner pipe is copper. The properties of pure kerosene and Fe₃O₄ are provided in Table 2.

Table 2: Properties of kerosene	and Fe ₃ O ₄	[17, 18]
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	$\rho(kg/m^3)$	$C_p(j/kg.k)$	k(W/m.k)	$d_p(nm)$	$\sigma(\Omega.m)^{-1}$	$\mu(kg/m.s)$]	$\beta[1/K]$
Kerosene (pure)	788	2010	0.129	-	5e-11	0.00164	800e-6
Fe ₃ O ₄	5200	670	6	47	25000	-	1.3e-5



Fig. 1: Cross-section view and mesh distribution of the enclosure filled with kerosene-Fe₃O₄.

2. Mathematical Modelling and Boundary Conditions

In this study, it is assumed that the flow is laminar and steady, and the MNF is incompressible. In addition, the effect of Brownian motion is neglected. To simulate the heat transfer through the magnetic nanofluid and assuming Boussinesq approximation, we derived the conservation of mass, momentums and energy equations as follow:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}$$

where *u* and *v* are the velocity vectors in the x and y direction, respectively

$$\rho_{nf}(u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} + u\frac{\partial v}{\partial x} + v\frac{\partial v}{\partial y}) = -\frac{\partial P}{\partial x} - \frac{\partial P}{\partial y} + \mu_{nf}(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2})$$

$$+\mu_0 M(\frac{\partial H}{\partial x} + \frac{\partial H}{\partial y}) + \sigma_{nf}(B_x B_y v + B_x B_y u - B_y^2 u - B_x^2 v)$$

$$\rho_{nf} C_{p_{nf}}(u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y}) = k_{nf}(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2}) - \mu_0 T \frac{\partial M}{\partial T}(u\frac{\partial H}{\partial x} + v\frac{\partial H}{\partial y})$$

$$+\mu_{nf}[2(\frac{\partial u}{\partial x})^2 + 2(\frac{\partial v}{\partial y})^2 + (\frac{\partial v}{\partial x} + \frac{\partial u}{\partial y})^2]$$

$$(2)$$

$$(3)$$

Note that the last two terms in Eq. 2 are the magnetization force and Lorentz force which occur between the ferromagnetic particle in the presence of magnetic field.

$$M = KH(T_{cu} - T) \tag{4}$$

where K is a constant, H is magnetic field intensity, T is the temperature of MNF, and T_{cu} is Curie temperature., The Lorentz force that depends on the electrical conductivity of the MNF and velocity of nanoparticles, is calculated as follows:

$$B = \mu_0(M + H) \tag{5}$$

where μ_0 is the magnetic permeability of vacuum $(4\pi \times 10^{-7})$, H is the magnetic field intensity (*A/m*), and *B* is magnetic flux density (*T*). In order to solve the magnetic field inside the enclosure in this study, Maxwell's equations are used as follow:

$$\nabla \mathbf{B} = \mathbf{0} \tag{6}$$

$$\nabla \times \mathbf{H} = 0 \tag{7}$$

$$\mathbf{E} = \mathbf{V} \times \mathbf{B}; \mathbf{J} = \boldsymbol{\sigma} \mathbf{E}$$
⁽⁸⁾

$$\mathbf{F} = \mathbf{J} \times \mathbf{B} \tag{9}$$

Finite element method with higher mesh density along the boundaries is used to solve the governing equations. In our simulation we assumed no slip-velocity condition on the walls. Hot surface is the copper pipe where the hot fluid passes through it and cold surface is glass. Having steady two phase flow inside the enclosure and isothermal condition on top and the bottom of the enclosure, we have the following boundary conditions:

$$\begin{cases} x = R_{in}, 0 < y < L: & u = o, v = o, T = T_h \\ x = R_{out}, 0 < y < L: & u = o, v = o, T = T_c \\ y = 0, 0 < x < r: & u = o, v = 0, \frac{\partial T}{\partial y} = 0 \\ y = L, 0 < x < r: & u = 0, v = 0, \frac{\partial T}{\partial y} = 0 \end{cases}$$
(10)

where *L* is the height of the enclosure (3.5 inch) and the radial distance between the inner pipe and the outer acrylic glass is 22.24 mm ($R_{out} - R_{in}$). Using polynomial curve fitting, we obtained the thermal conductivity as a function of volume fraction ϕ and magnetic field H from the literature [19]. In our study, we chose five different volume fractions (1.115%, 1.7%, 2.23%, 3.465%, and 4.7%) for numerical investigation. To compare and validate our simulation results with previous studies in which Ra versus Nu is provided (no magnetic field and no nanoparticles), we defined the Rayleigh

number as $Ra = \frac{g\beta\Delta TL^3}{v\alpha}$ and the Nusselt number on the hot surface as follows:

$$Nu_{\text{local}} = \frac{hL}{k_f} \tag{11}$$

where *L* is effective length and h is the heat transfer coefficient $(h = \frac{q_n}{T_h - T_c})$. q_n is normal heat flux from the wall and can also be expressed as $q_n = -k_{nf} \left(\frac{\partial T}{\partial X}\right)$. Finally, we calculated the average Nusselt number along the hot wall as follows:

$$\overline{Nu} = \frac{1}{L} \int_0^L -\left(\frac{k_{nf}}{k_f}\right) \frac{\partial T}{\partial X} dY$$
(12)

3. Results and Discussions

In order to validate the numerical scheme and accuracy of the simulation, the Nusselt number is plotted versus Rayleigh number, when the Prandlt number (Pr) is about 0.7. The results show the good agreement when compared with available literatures in the Fig. 2.



Fig. 2: Nusselt number versus Rayleigh number for the present study compared with other literatures ($\phi = 0$, H = 0, and Pr=0.7).



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Fig. 3-Fig. 8 show the effect of magnetic field on Nusselt number when Rayleigh is changing from 10^2 to 10^2 for various volume fractions of nanoparticle in kerosene. As can be seen from Fig. 3-Fig. 8 increasing the magnetic field with higher volume fraction results in increasing Nu markedly. From Fig. 3- Fig. 8, there is a slight decrease observed for high

volume fraction approximately at 70×10^3 [A/m]; this can be explained due to the atomic motion of the particles and/or induction heating occurred inside the enclosure. To investigate the change of the Nu versus Ra for various magnetic field, Fig 9 and Fig 10 are provided below for two specific volume fractions ($\phi = 1.115\%$ and $\phi = 4.7\%$).



Fig. 11 and Fig. 12 illustrate the temperature distribution (steady-state) for different Rayleigh number when ϕ is constant ($\phi = 4.7\%$). The uniform conduction like temperature distribution is observed in the Fig. 11 when Ra is 10^2 compared to Fig. 12 when Ra increased.



Fig. 11: Temperature distribution (Ra= 10^2 , $\phi = 4.7\%$, and H= 80×10^3 [A/m]).



Fig. 12: Temperature distribution (Ra=10⁷, $\phi = 4.7\%$, and H=80 × 10³ [A/m]).

In addition, the velocity of flow is being affected due to the Lorentz force induced in the MNF in the presence of applied magnetic field. Thus, we defined dimensionless velocity to discuss this phenomena as follows [20]:

$$\delta_T \sim LRa^{-1/4} \tag{13}$$

$$v \sim \frac{\alpha_{nf}}{L} R a^{1/2} \tag{14}$$

where δ_T is the thermal thickness and α_{nf} is a thermal diffusivity of MNF which is related to thermal conductivity (*k*); and *k* itself, as previously discussed, is the function of magnetic field. The calculated velocity is divided by reference velocity (Eq. 14) and plotted along the radial distance of the enclosure.



Fig. 13: Dimensioneless velocity along the radial distance for different ϕ



Fig. 14: Velocity field and velocity vectors for Ra=10⁶, H=20 × 10³ [A/m], $\phi = 2.23\%$.

Fig. 15 shows the effect of magnetic forces on the MNF for different Ra numbers. It can be concluded that for higher Ra number, the effect of the magnetic force is significant and this force can destabilizes the fluid equilibrium and change the temperature gradient accordingly.



Fig. 15: Temperature distribution and magnetization contour (\$\phi=4.7%, H=80 \times 10^3 [A/m]).

4. Conclusion

In this paper, we investigated the effect of transverse magnetic field on an annular enclosure filled with magnetic nanofluid. A nonlinear relationship between thermal conductivity and magnetic field was obtained and used in the properties of MNF. Finite element method was utilized with high mesh density near boundaries to determine the heat transfer in magnetic nanofluid assuming laminar flow and steady-state. The results show increasing the magnetic field strength and Rayleigh number both lead to increasing the Nusselt number, significantly.

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